

Numerical Simulation of Turbulent Flows

Helfried Steiner

Conex Kick-off Meeting

Sofia, 01/11/2003



Overview

- **Turbulent motion characteristics**
 - Unstable flow
 - Turbulent eddies, length scales
 - Turbulent Energy spectrum
 - Kolmogorov's theory
- **Computation of turbulent flow**
 - Direct Numerical Simulation
 - Reynolds Averaged Numerical Simulation
 - Large-Eddy Simulation
- **Examples**
- **Resume**



Turbulent Motion Characteristics

Reynolds number :

$$\text{Re} = \frac{\text{inertial forces}}{\text{viscous forces}} \geq \text{Re}_{krit}$$

$\text{Re} \geq \text{Re}_{krit}$:  **Flow unstable**  **Transition to turbulent motion**

Turbulent motion : all flow quantities φ fluctuate

 **motion= unsteady & 3-dimensional !**

$$\varphi = \varphi (x_1, x_2, x_3, t)$$

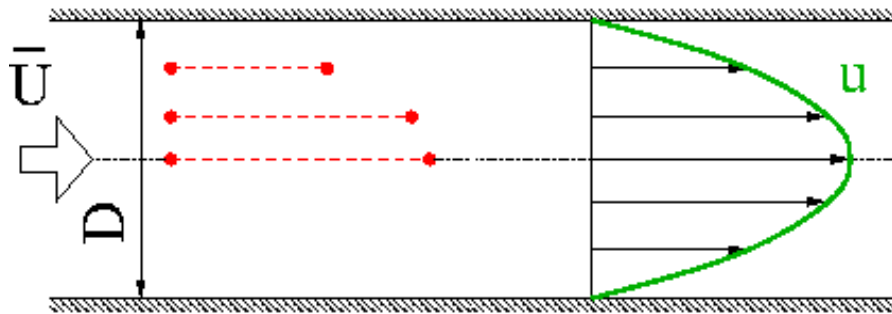


Turbulent Motion Characteristics

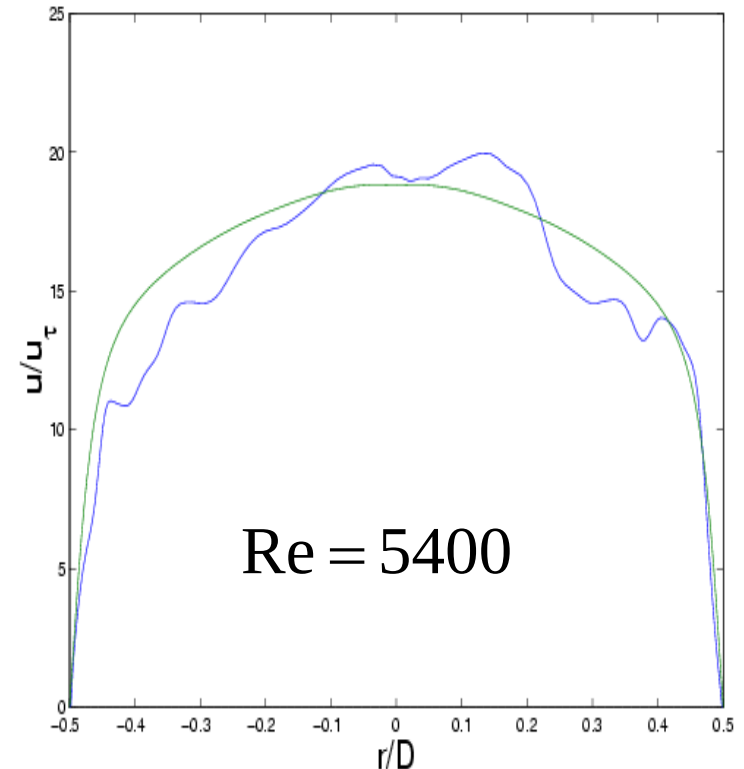
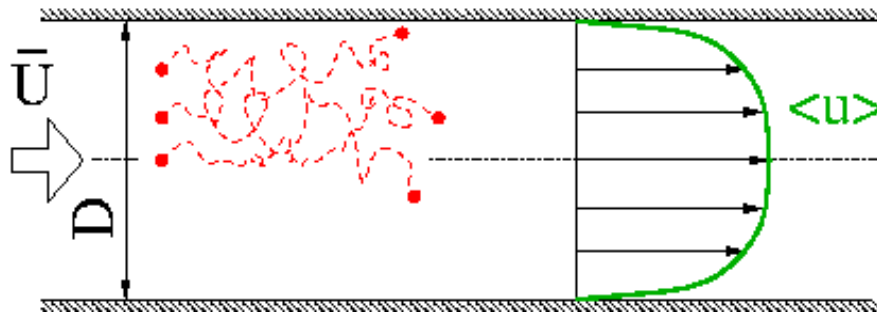
Flow through a cylindrical pipe:

$$Re_{krit} \approx 2300$$

$$Re < Re_{krit}$$



$$Re > Re_{krit}$$

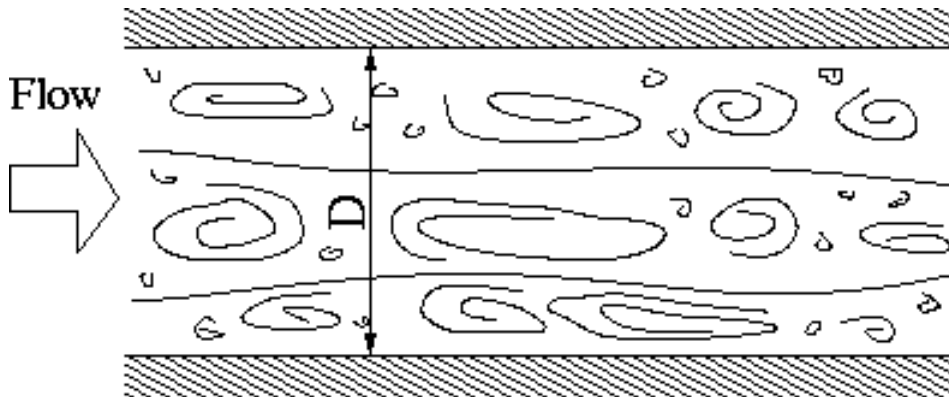


Turbulent Motion Characteristics

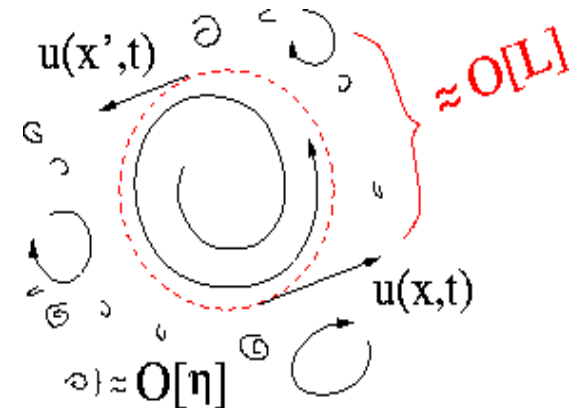
Fluctuating motion characterized by eddies of different sizes:

➡ **turbulent length scales**

Turbulent pipe flow:



turbulent eddies



Turbulent Motion Characteristics

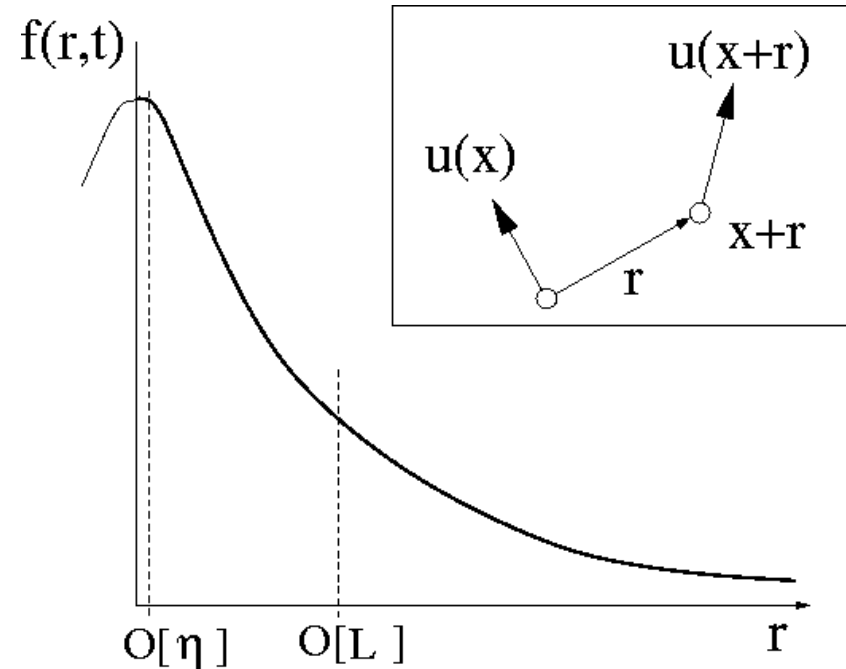
Length scales

correlation:

$$f(r,t) = \frac{\langle u(x,t) u(x+r,t) \rangle}{\langle u(x,t)^2 \rangle}$$

Integral scale :

$$L = \int_0^{\infty} f(r,t) dr$$



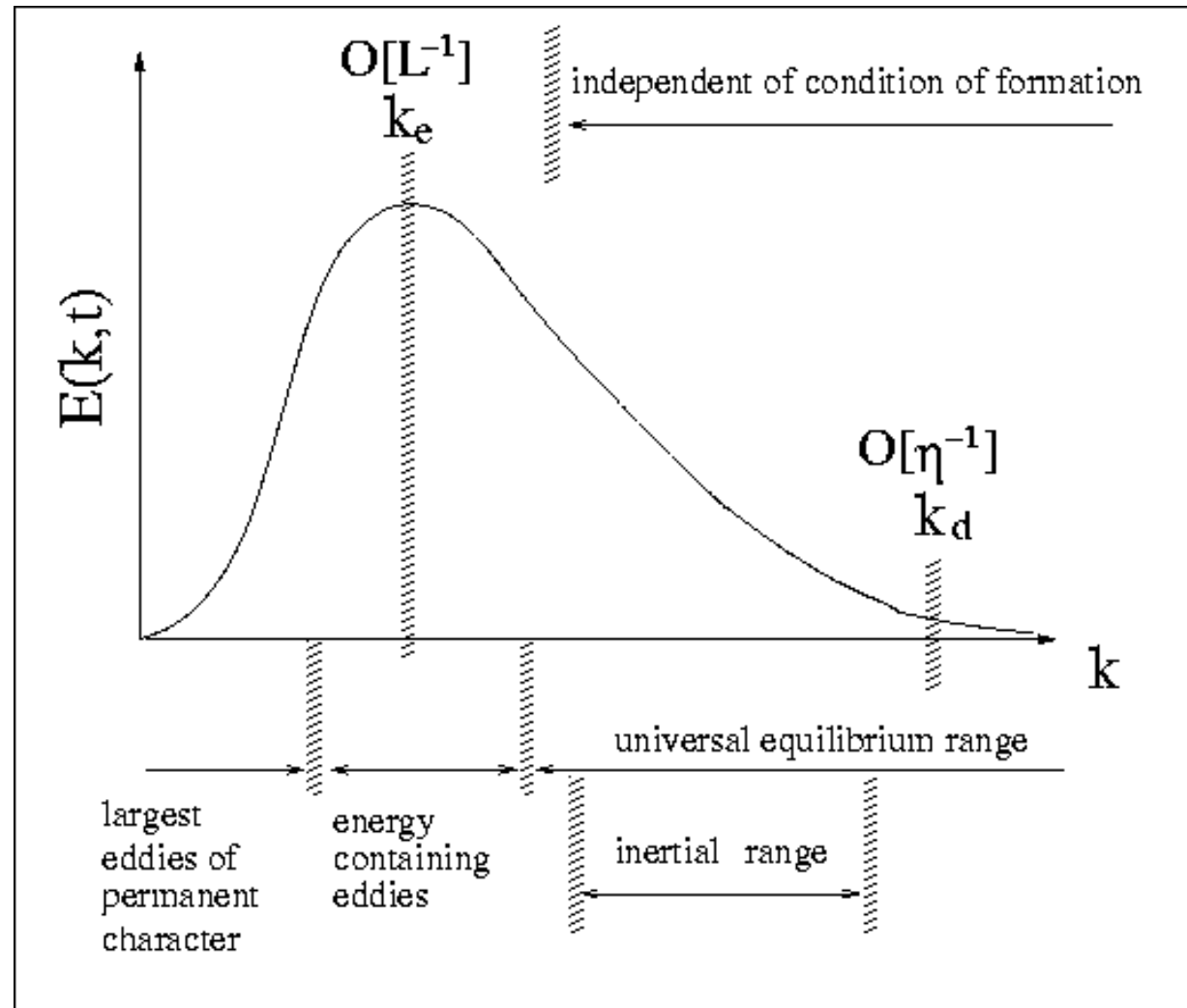
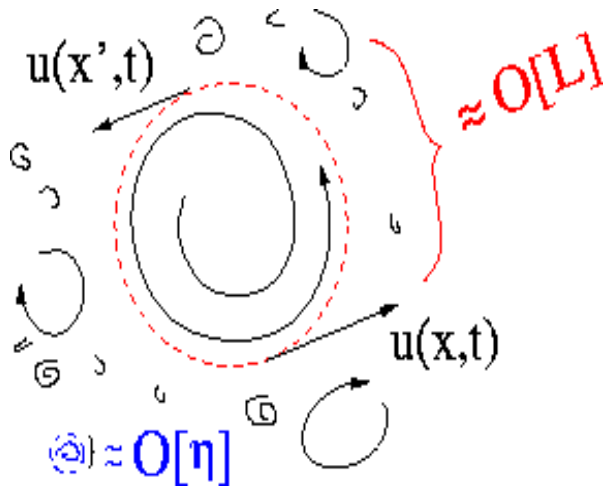
Kolmogorov scale:

$$\eta = \left(\frac{\nu^3}{\varepsilon} \right)^{1/4}, \quad \varepsilon = \left\langle \nu \frac{\partial u_i}{\partial x_j} \frac{\partial u_i}{\partial x_j} \right\rangle$$



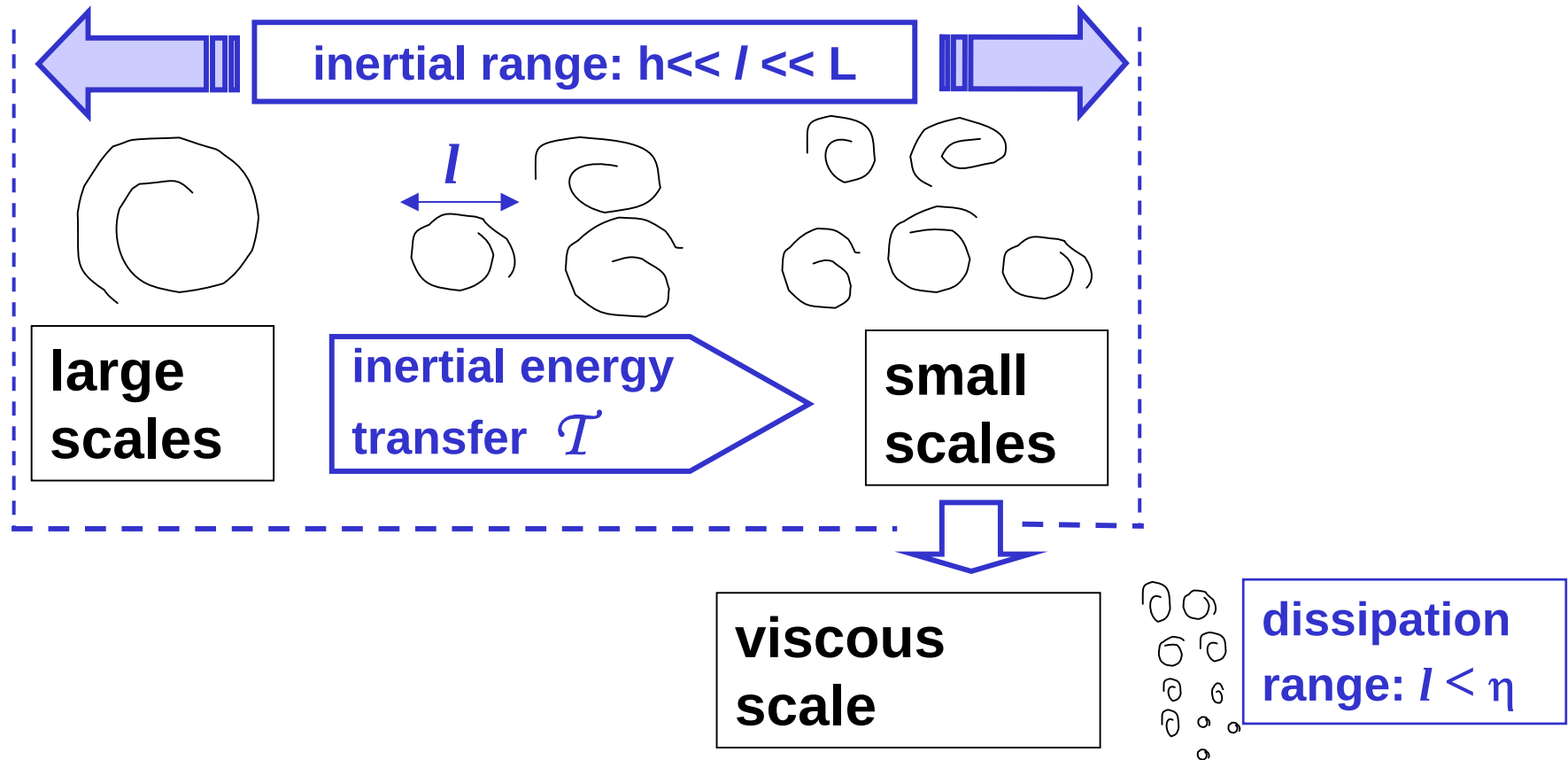
Turbulent Motion Characteristics

Turbulent Energy Spectrum



Turbulent Motion Characteristics

Kolmogorov's eddy cascade hypothesis (1941):

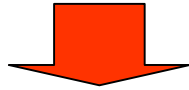


Turbulent Motion Characteristics

Inertial Range: $\eta \ll l \ll L$:

turbulent energy transfer at all length scales $l = 1/k$
depends **only** on the **scale invariant** dissipation

$$\mathcal{T}(l) = \varepsilon = \text{const.}$$



Important for Turbulence Modeling!!

Viscous range: $l < \eta$

dissipation ε + **viscosity** ν



Computation of turbulent flows

Conservation equations:

Mass:
$$\frac{\partial \rho u_j}{\partial x_j} = 0$$

Momentum:

$$\frac{\partial \rho u_i}{\partial t} + \frac{\partial \rho u_i u_j}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left[\mu \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) - \mu \frac{2}{3} \delta_{ij} \frac{\partial u_m}{\partial x_m} \right]$$

Scalar Φ_k :

$$\frac{\partial \rho \Phi_k}{\partial t} + \frac{\partial \rho u_j \Phi_k}{\partial x_j} = \frac{\partial}{\partial x_j} \left(\rho D \frac{\partial \Phi_k}{\partial x_j} \right) + \Omega_k$$



Computation of turbulent flows

Direct Numerical Simulation (DNS)

- Resolves all relevant scales down to Kolmogorov scale η
- no turbulence model needed
- provides full turbulence statistics
- high resolution and accuracy required ($N_p \sim Re^{9/4}$)
- restricted to low Re numbers flow due to exceeding computational cost



Computation of turbulent flows

Reynolds Averaged Numerical Simulation (RANS)

Statistical approach tracking the (Reynolds) averages over ensemble N

$$\langle f \rangle(\vec{x}, t) = \lim_{N \rightarrow \infty} \frac{1}{N} \sum_{n=1}^N f_n(\vec{x}, t) \Rightarrow \langle u_i \rangle, \langle p \rangle, \langle \Phi_k \rangle, \dots$$

Reynolds decomposition:

$$u_i = \langle u_i \rangle + u'_i$$
$$p = \langle p \rangle + p'_k$$
$$\Phi_k = \langle \Phi_k \rangle + \Phi'_k$$



Computation of turbulent flows

➔ Reynolds averaged equations (case $\rho = \text{const.}$):

$$\frac{\partial \langle u_j \rangle}{\partial x_j} = 0$$

$$\frac{\partial \langle u_i \rangle}{\partial t} + \frac{\partial \langle u_i \rangle \langle u_j \rangle}{\partial x_j} = -\frac{1}{\rho} \frac{\partial \langle p \rangle}{\partial x_j} + \frac{\partial}{\partial x_j} \left(\frac{\mu}{\rho} \frac{\partial \langle u_i \rangle}{\partial x_j} \right) - \frac{\partial \langle u'_i u'_j \rangle}{\partial x_j}$$

$$\frac{\partial \langle \Phi_k \rangle}{\partial t} + \frac{\partial \langle u_j \rangle \langle \Phi_k \rangle}{\partial x_j} = \frac{\partial}{\partial x_j} \left(D \frac{\partial \langle \Phi_k \rangle}{\partial x_j} \right) - \frac{\partial \langle u'_j \Phi'_k \rangle}{\partial x_j} - \left\langle \frac{\Omega_k}{\rho} \right\rangle$$



Computation of turbulent flows

➔ Model required for unclosed nonlinear terms:

$$\langle u'_i u'_j \rangle = -\boxed{\nu_t} \left(\frac{\partial \langle u_i \rangle}{\partial x_j} + \frac{\partial \langle u_j \rangle}{\partial x_i} \right) + \frac{\delta_{ij}}{3} \langle u'_m u'_m \rangle$$

$$\langle u'_j \Phi'_k \rangle = -\boxed{D_t} \frac{\partial \langle \Phi_k \rangle}{\partial x_j}$$

ν_t, D_t modeled ,e.g., with $k - \varepsilon$ - model

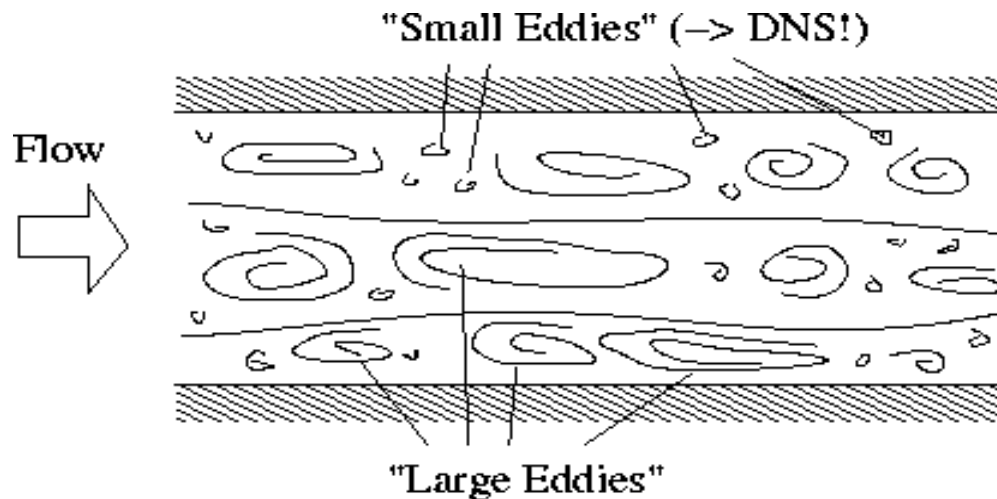
$$\nu_t = C_\mu \frac{k^2}{\varepsilon}, \quad D_t = \frac{\nu_t}{Sc_t} \quad \text{where} \quad k = \frac{1}{2} \langle u'_m u'_m \rangle$$



Computation of turbulent flows

Large Eddy Simulation (LES)

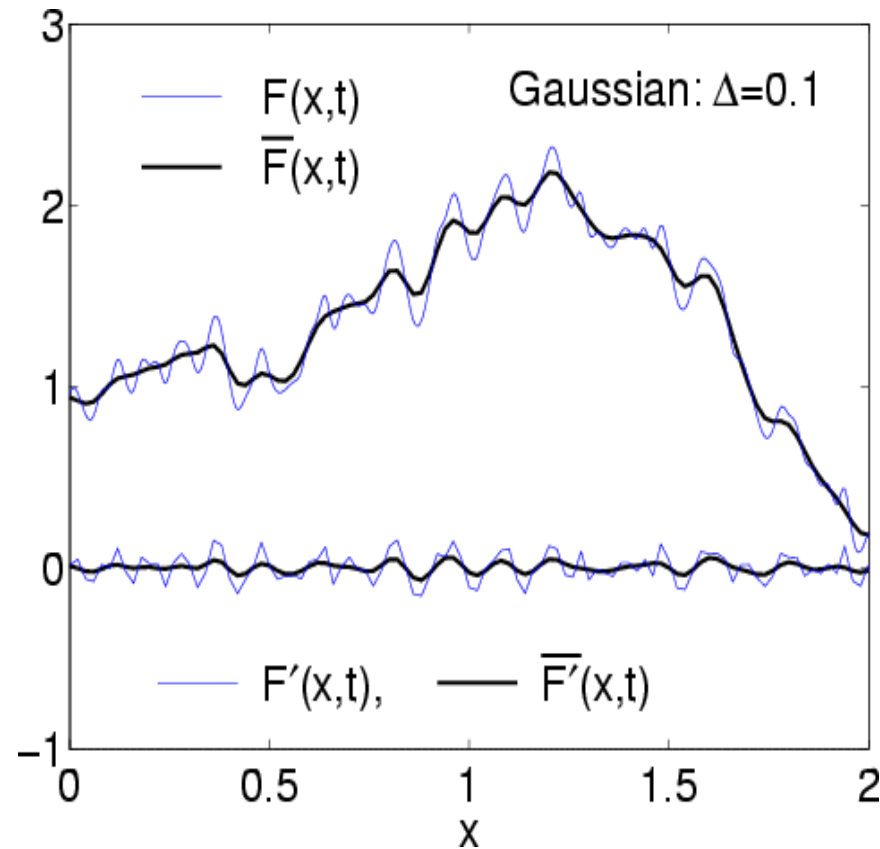
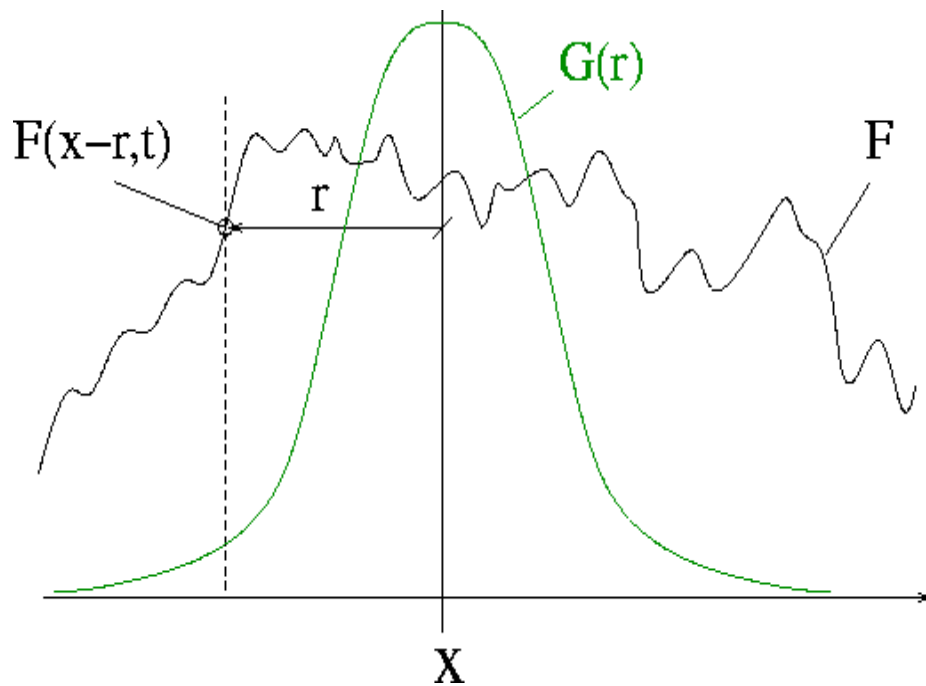
- LES resolves the unsteady 3-dimensional motion of the large structures
- small structures (subgrid-scale) are modeled



Computation of turbulent flows

Filter operation:  resolved structures

$$\bar{F}(\vec{x}, t) = \int_D F(\vec{x} - \vec{r}, t) G(\vec{r}) d\vec{r}$$



Computation of turbulent flows

Filter operation:  resolved structures

 filtered conservation equations (case $\rho=\text{const.}$)

$$\frac{\partial \bar{u}_j}{\partial x_j} = 0$$

$$\frac{\partial \bar{u}_i}{\partial t} + \frac{\partial \bar{u}_i \bar{u}_j}{\partial x_j} = -\frac{1}{\rho} \frac{\partial \bar{p}}{\partial x_j} + \frac{\partial}{\partial x_j} \left(\frac{\mu}{\rho} \frac{\partial \bar{u}_i}{\partial x_j} \right) - \frac{\partial}{\partial x_j} \underbrace{(\bar{u}_i \bar{u}_j - \bar{u}_i \bar{u}_j)}_{\tau_{ij}^R}$$

$$\frac{\partial \bar{\Phi}_k}{\partial t} + \frac{\partial \bar{u}_j \bar{\Phi}_k}{\partial x_j} = \frac{\partial}{\partial x_j} \left(D \frac{\partial \bar{\Phi}_k}{\partial x_j} \right) - \frac{\partial}{\partial x_j} \underbrace{(\bar{u}_j \bar{\Phi}_k - \bar{u}_j \bar{\Phi}_k)}_{\sigma_j^R} - \frac{\bar{\Omega}_k}{\rho}$$



Computation of turbulent flows

➔ Model required for unclosed SGS-terms:

$$\tau_{ij}^R - \frac{1}{3} \tau_{kk}^R \delta_{ij} = - \boxed{\nu_T} \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) = - 2 \nu_T \bar{S}_{ij}$$

$$\sigma_j^R = - \boxed{D_T} \frac{\partial \bar{\Phi}_k}{\partial x_j}$$

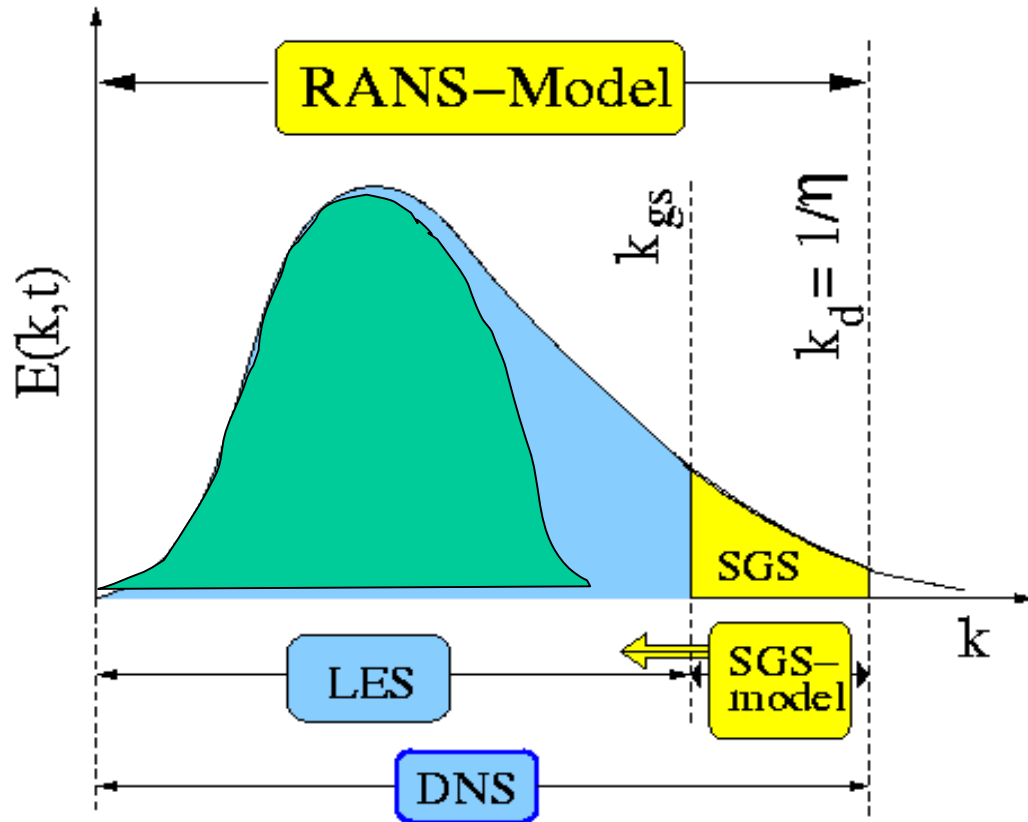
ν_T, D_T modeled ,e.g., with Smagorinsky-type models

$$\nu_T = (C_S \Delta)^2 |\bar{S}_{ij}|, \quad D_T = \frac{\nu_T}{Sc_T}$$



Computation of turbulent flows

Simulation methods in wave number space $k = l^{-1}$



Most standard models based on scale invariance of ε

Requires broad inertial range associated with $Re \gg 1$

Problem at low Re !

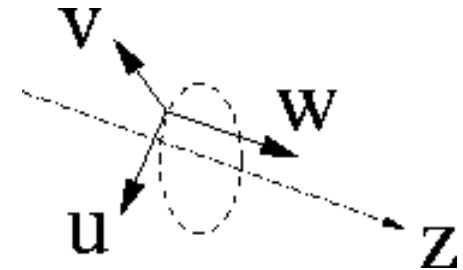
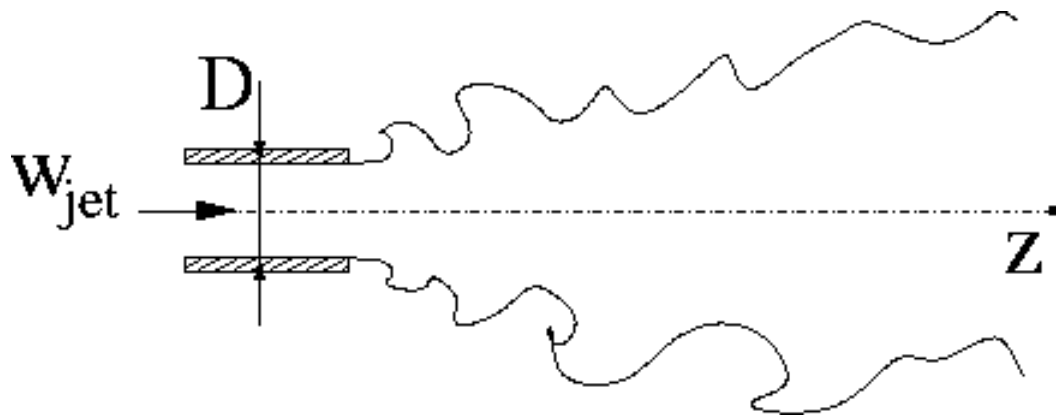


Examples

DNS of a turbulent cylindrical jet

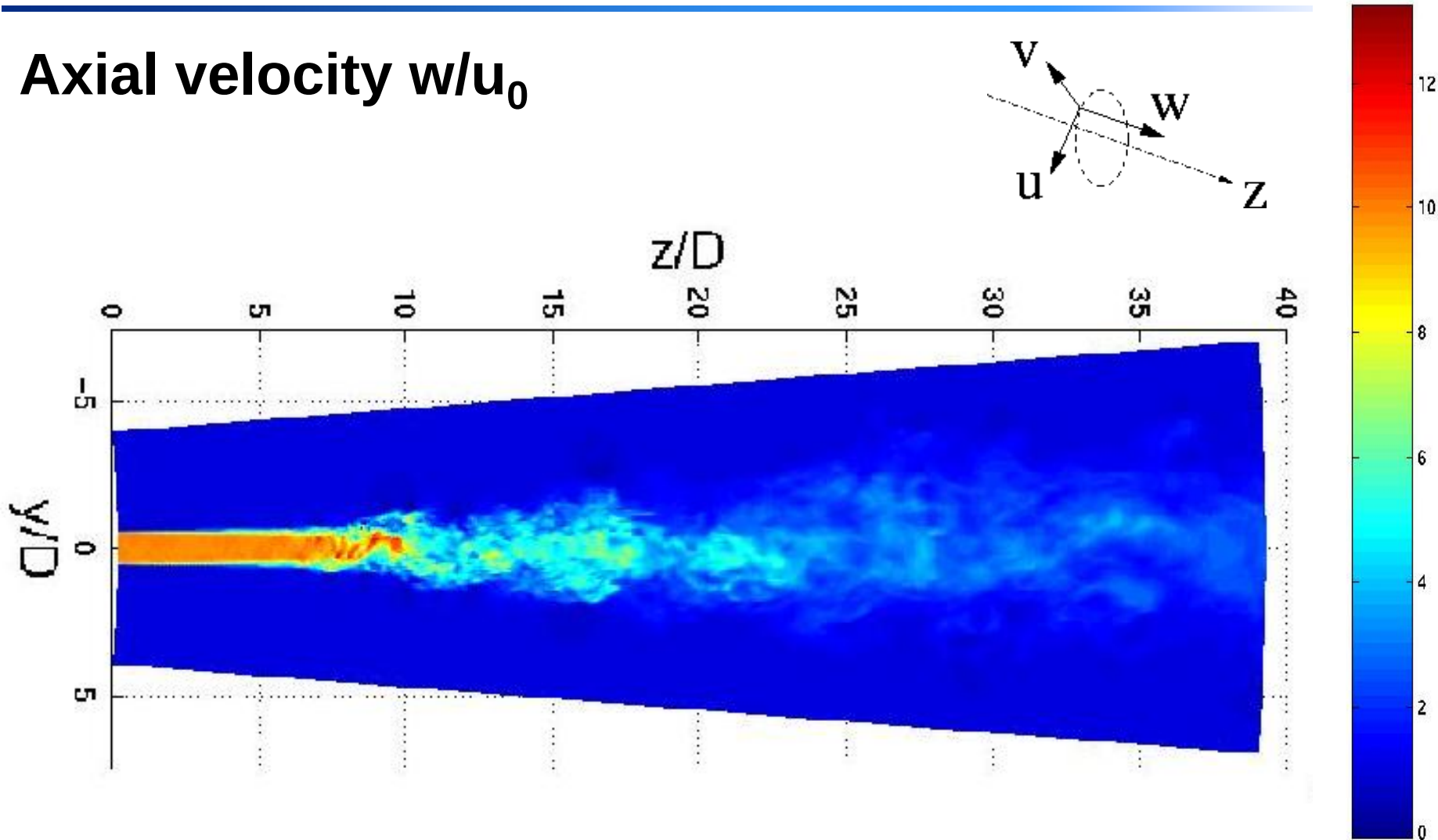
$$\text{Re} = \frac{w_{\text{jet}} D}{\nu} = 2400$$

Grid: $N_P \approx 1.2 \cdot 10^6$



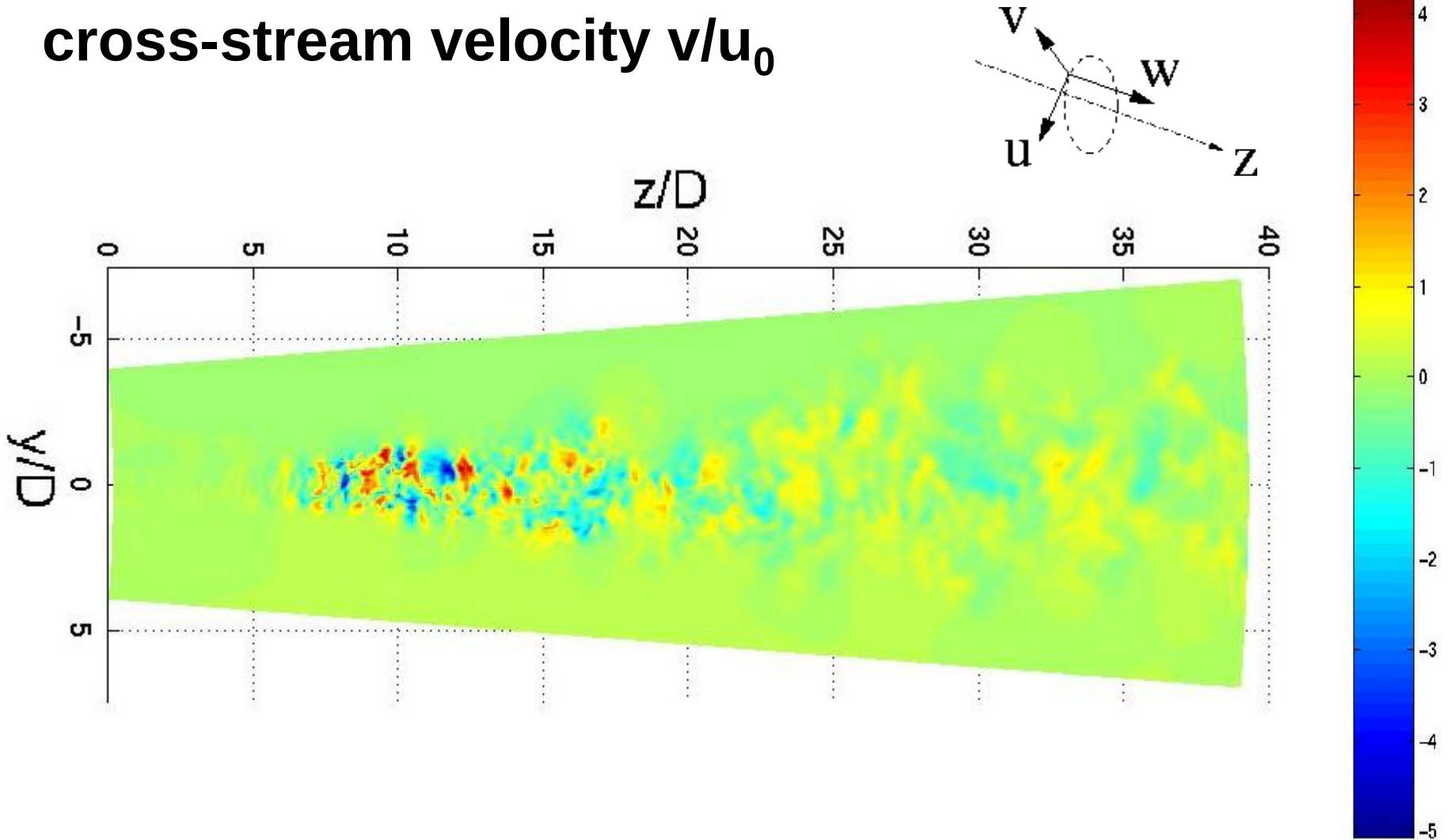
Examples *DNS of a turbulent cylindrical jet*

Axial velocity w/u_0



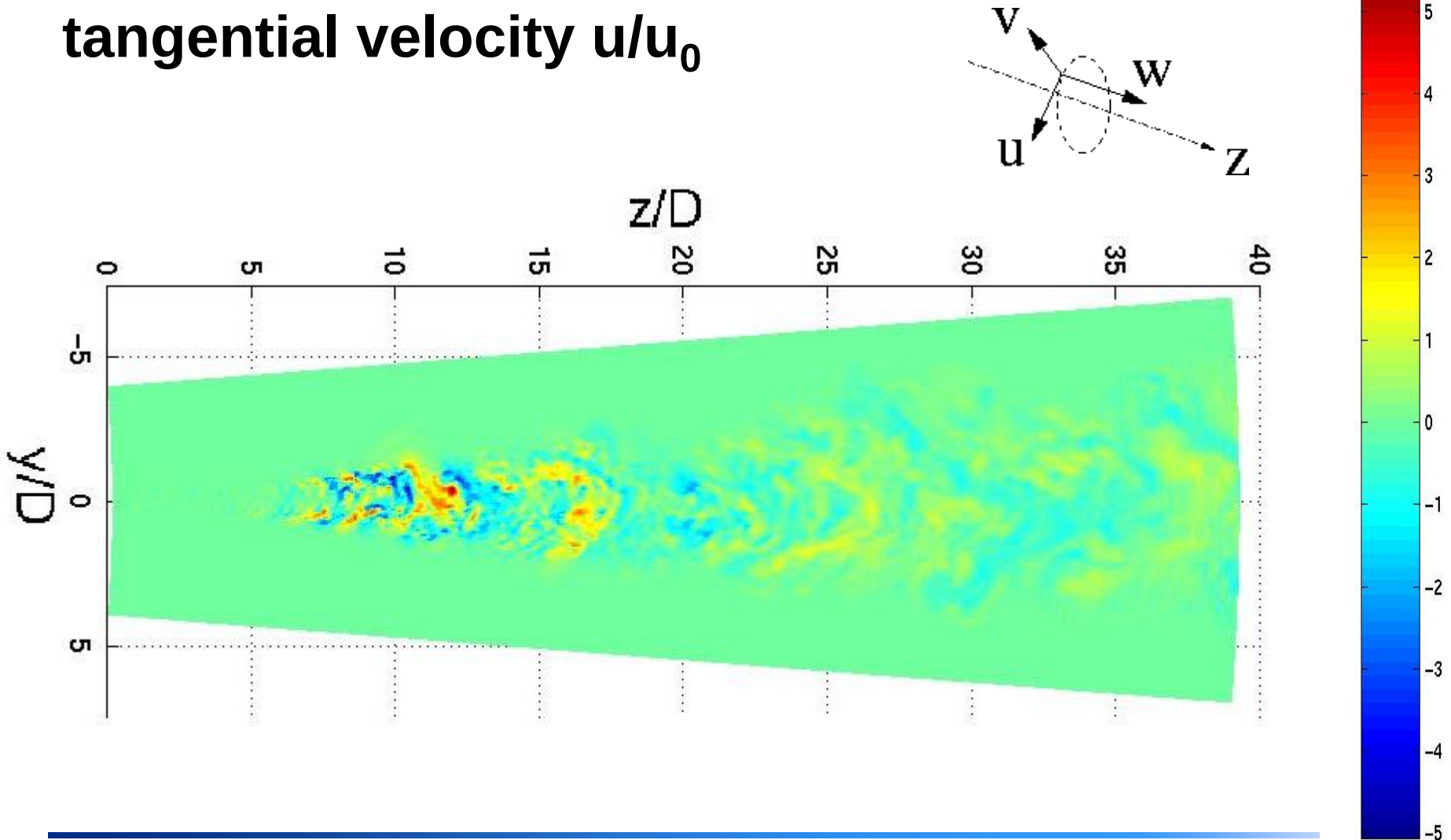
Examples *DNS of a turbulent cylindrical jet*

cross-stream velocity v/u_0



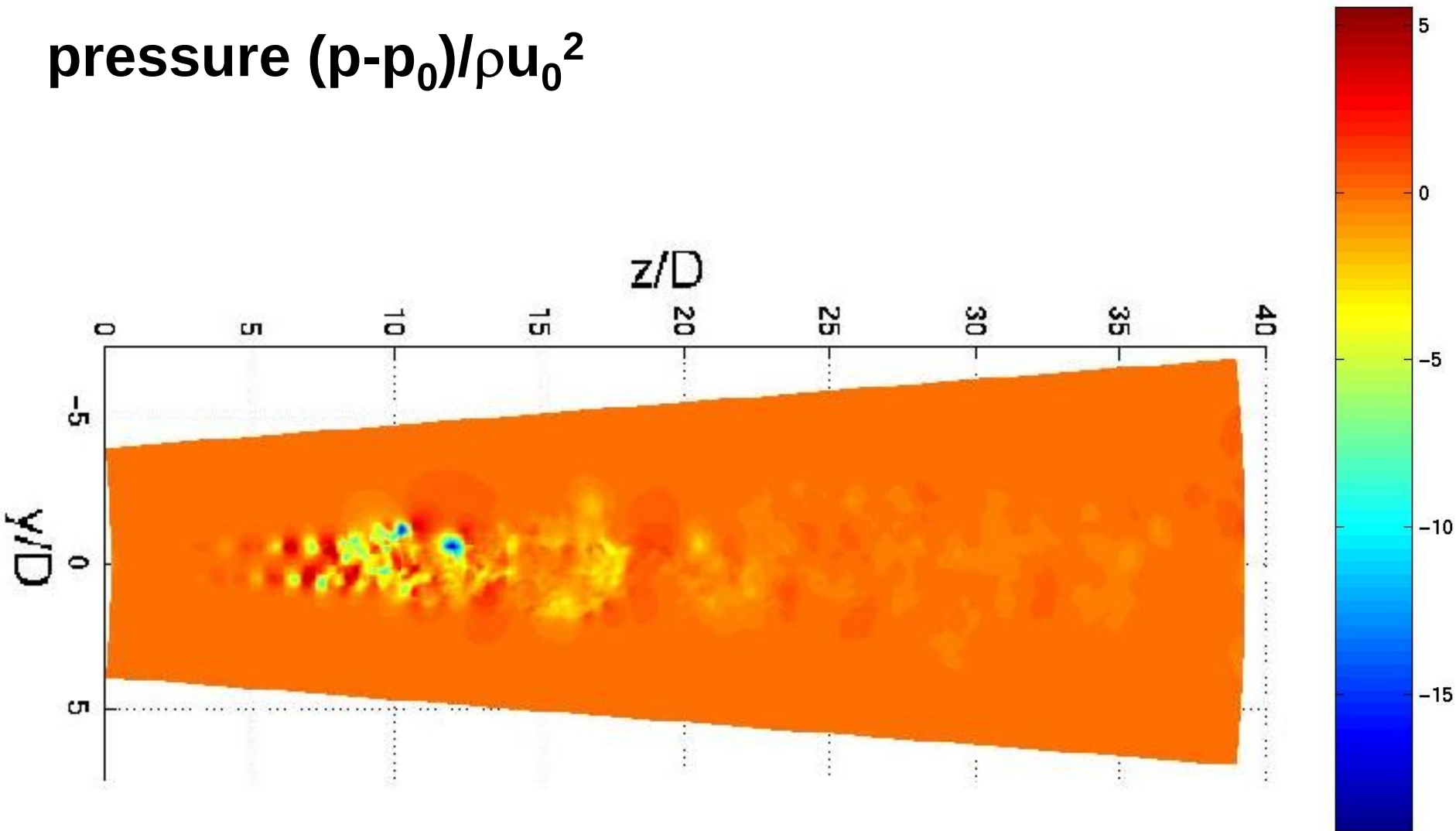
Examples *DNS of a turbulent cylindrical jet*

tangential velocity u/u_0



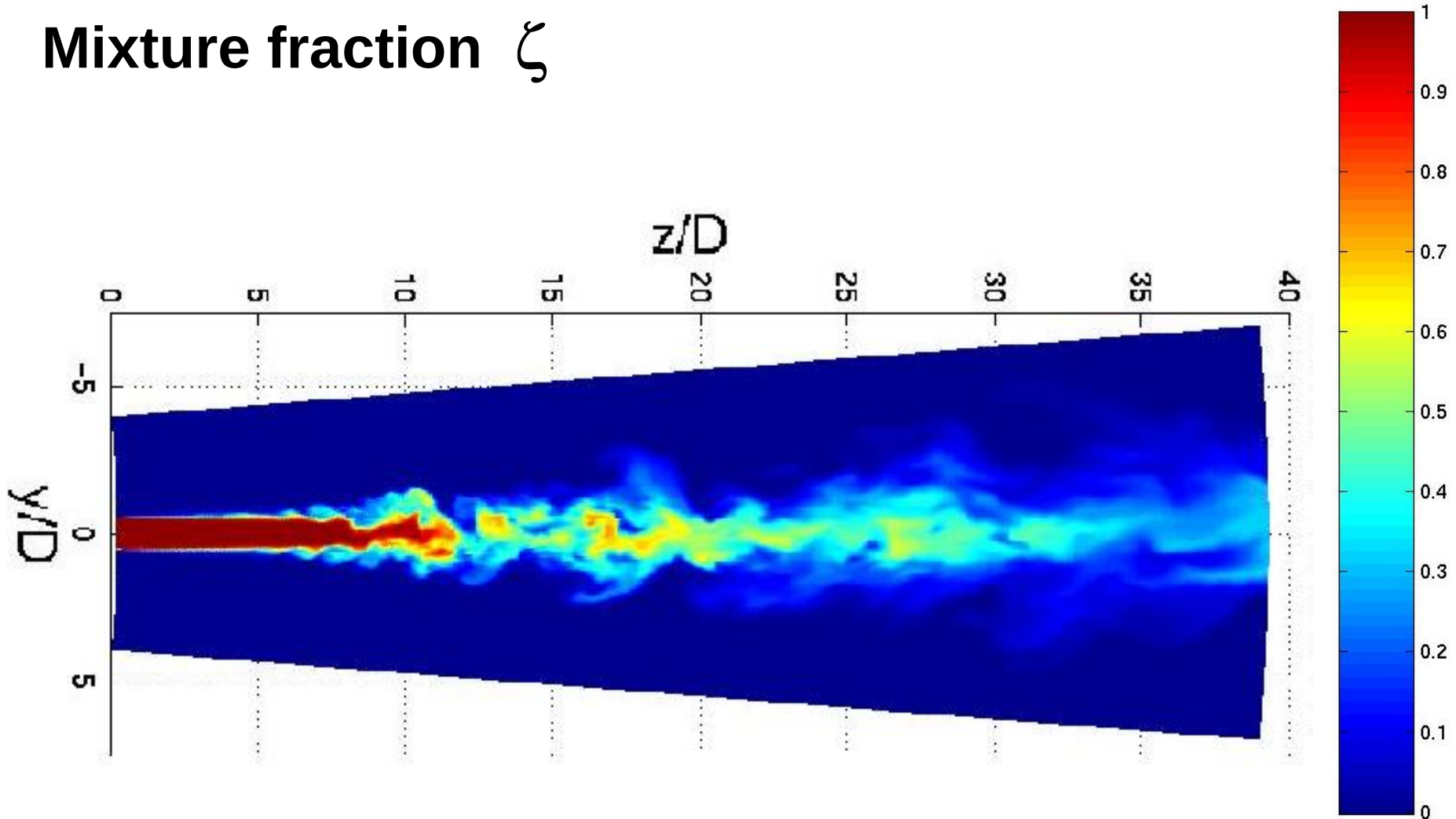
Examples *DNS of a turbulent cylindrical jet*

pressure $(p-p_0)/\rho u_0^2$



Examples *DNS of a turbulent cylindrical jet*

Mixture fraction ζ

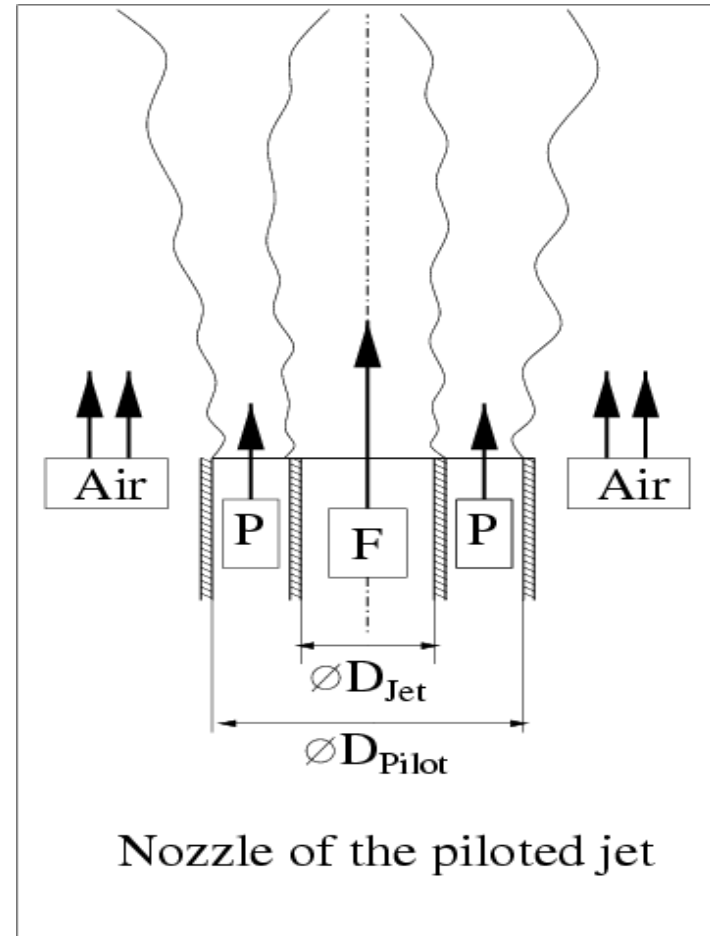


Examples *LES of a turbulent reacting jet*

LES of a methane-air jet flame (Sandia D flame)

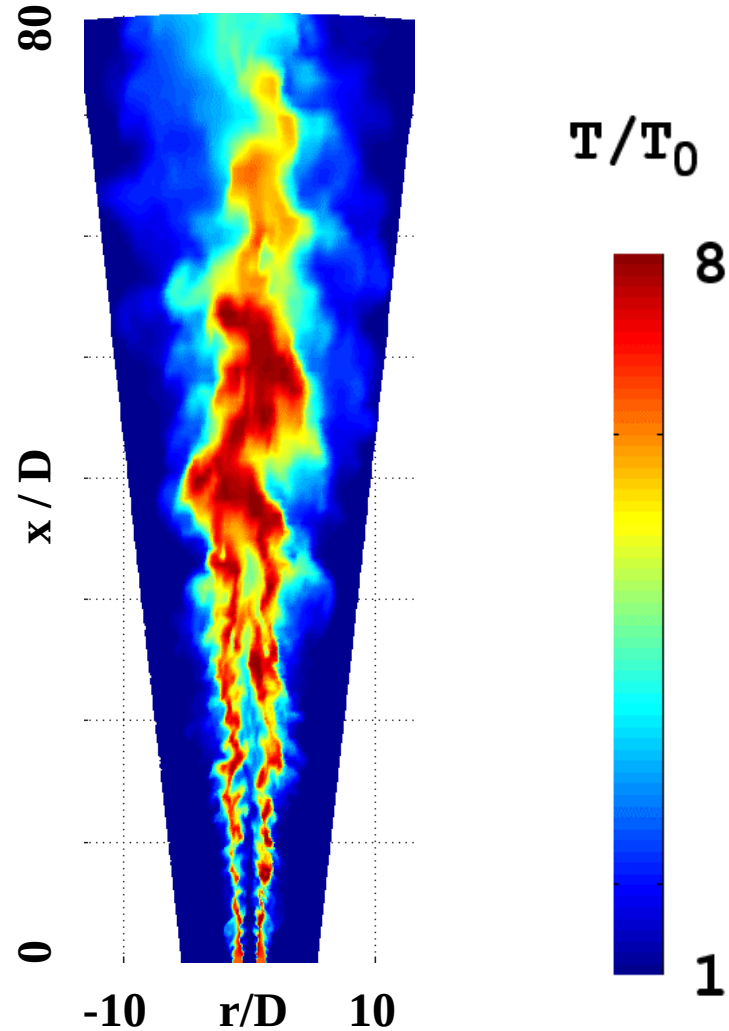
Piloted methane-air
diffusion flame

$$\text{Re} = \frac{w_{\text{jet}} D_{\text{jet}}}{\nu} = 22400$$



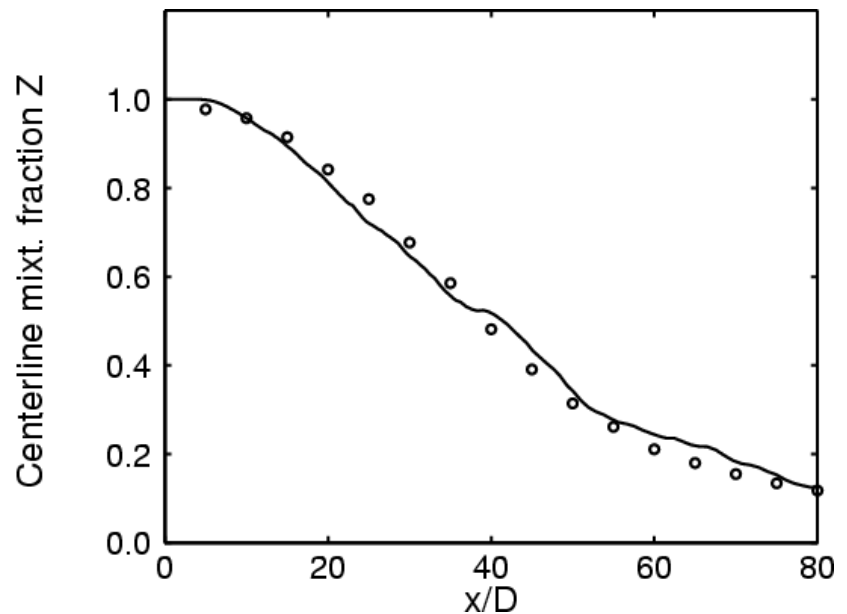
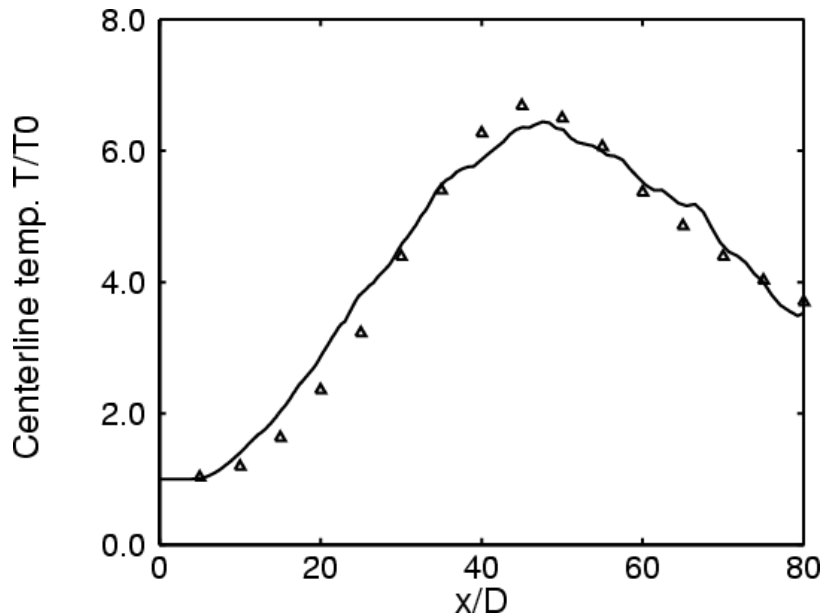
Examples *LES of a turbulent reacting jet*

Instantaneous
temperature field T/T_0
($T_0 = 293\text{K}$)



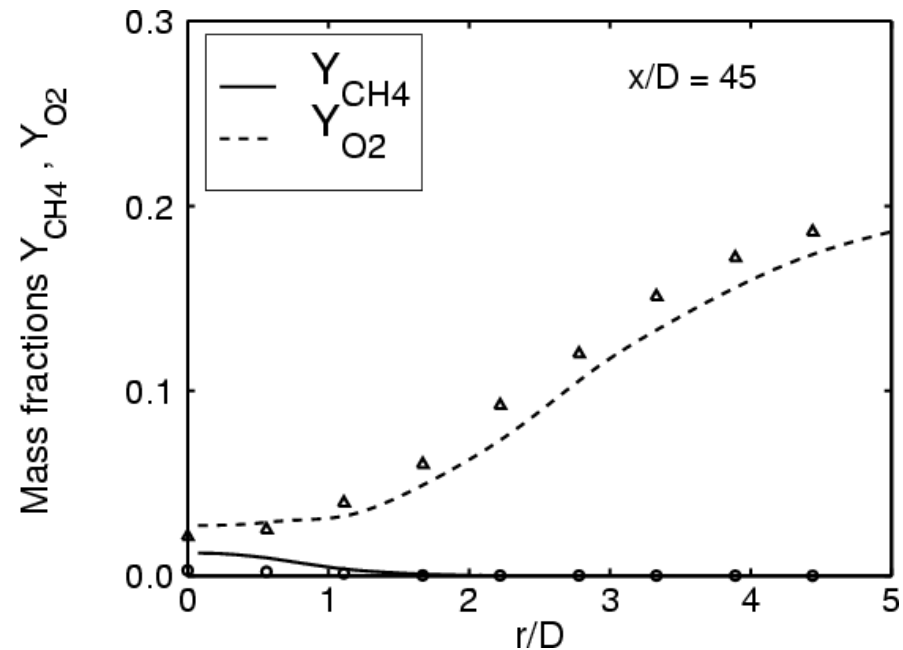
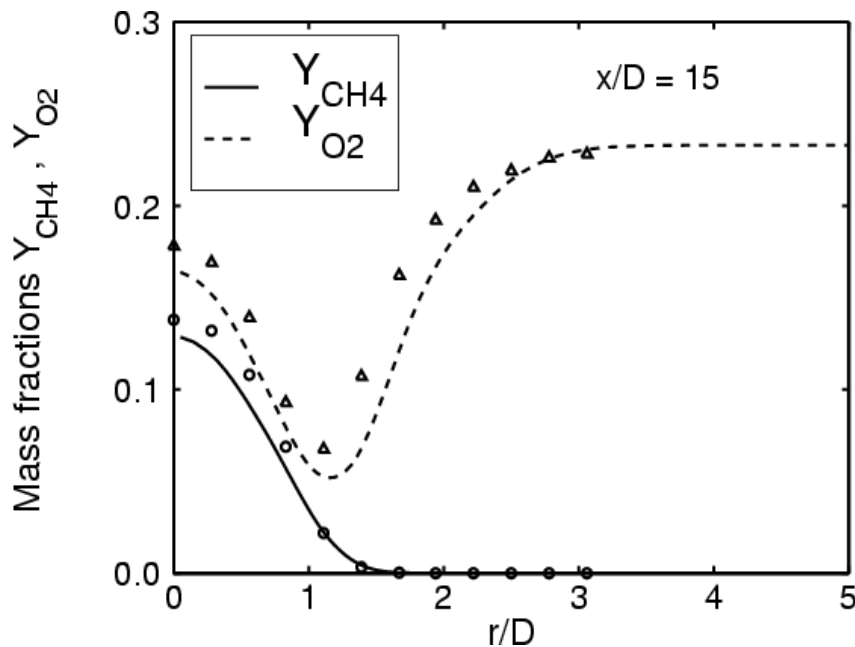
Examples *LES of a turbulent reacting jet*

Temperature T/T_0 and mixture fraction Z along centerline of the jet

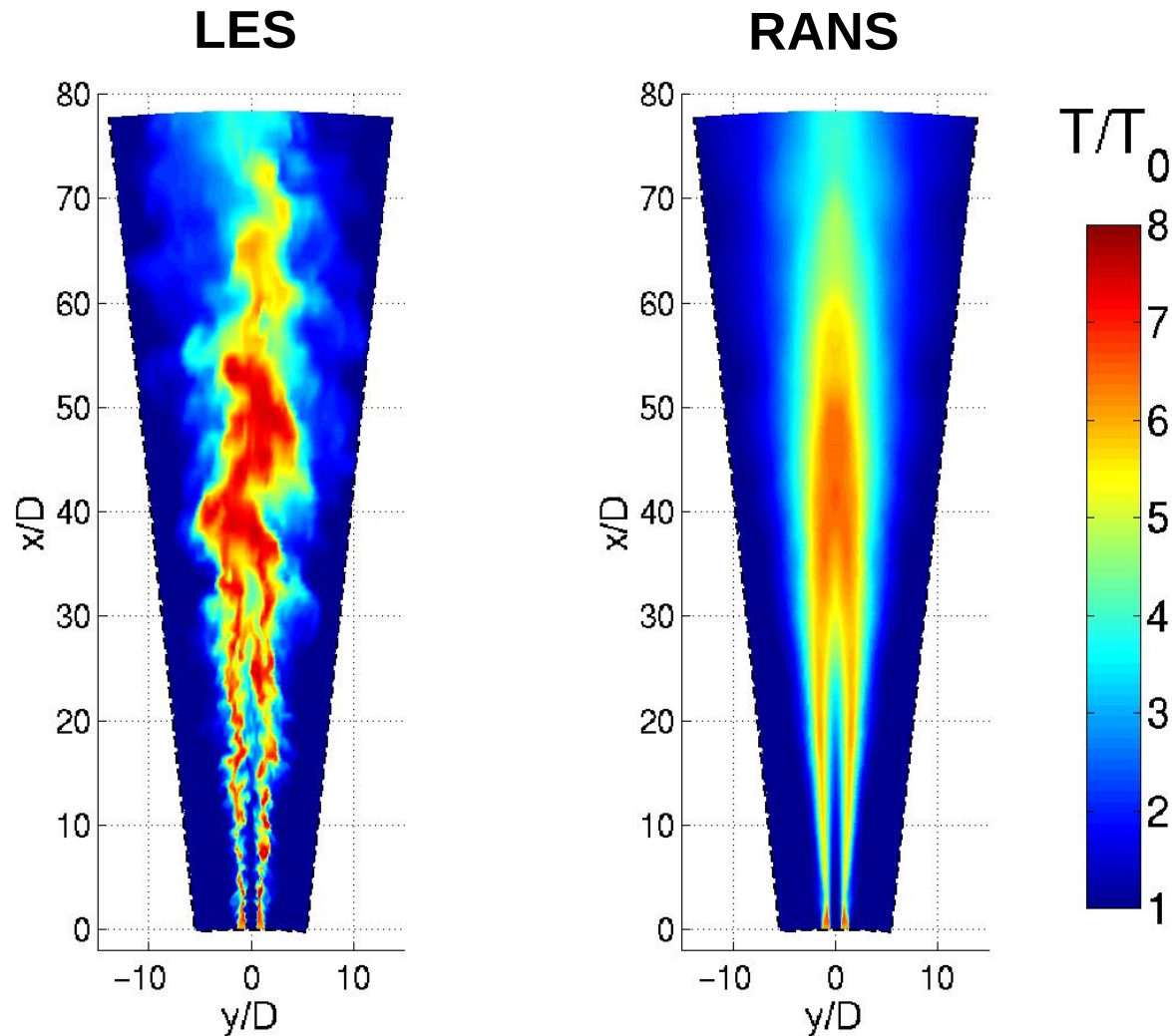


Examples *LES of a turbulent reacting jet*

Radial profiles of mass fractions Y_{CH_4} and Y_{O_2} at downstream locations $x/D=15$ and $x/D=45$



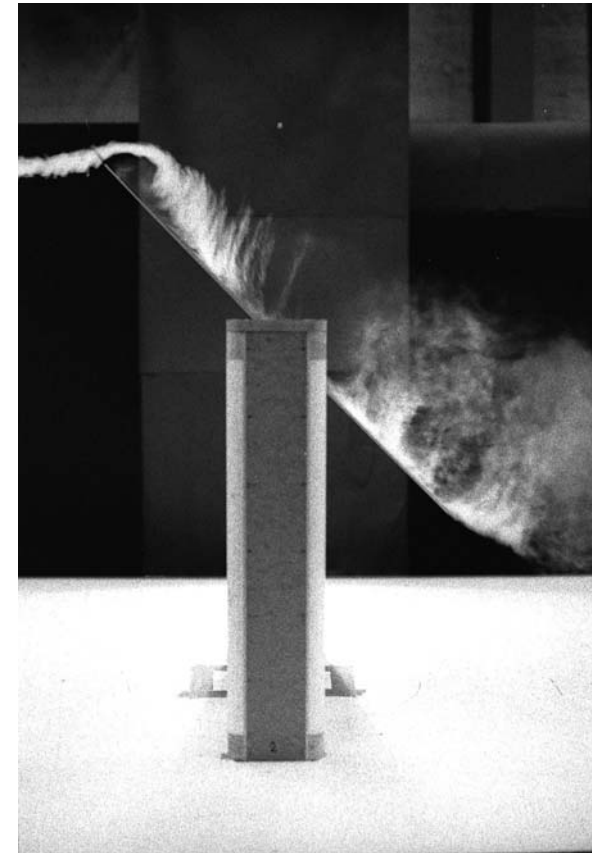
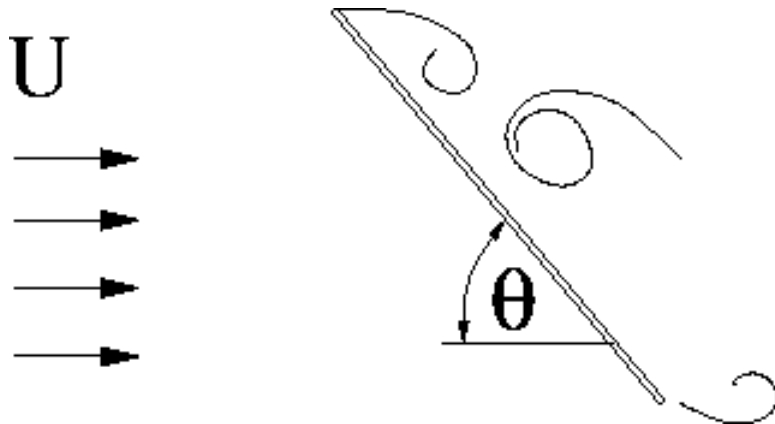
Examples *LES of a turbulent reacting jet : LES ↔ RANS*



Examples *RANS of flow around a flat plate*

RANS of flow around a flat plate with different angles of attack Θ

$$\text{Re} = \frac{U L_{\text{plate}}}{\nu} = 1.9 \cdot 10^6$$

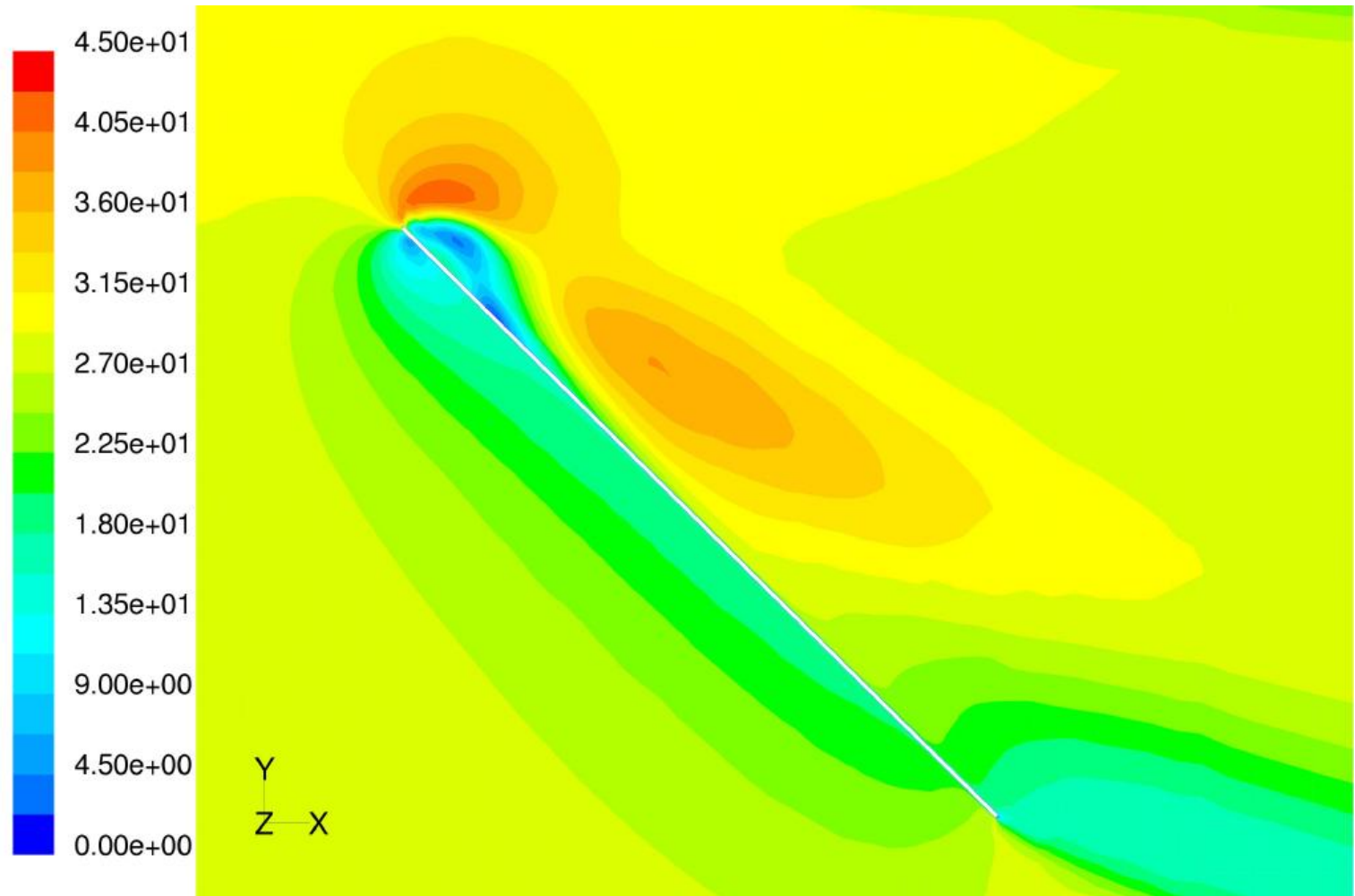


Turbulence model : k- ϵ (Code: FLUENT)



Examples *RANS of flow around a flat plate*

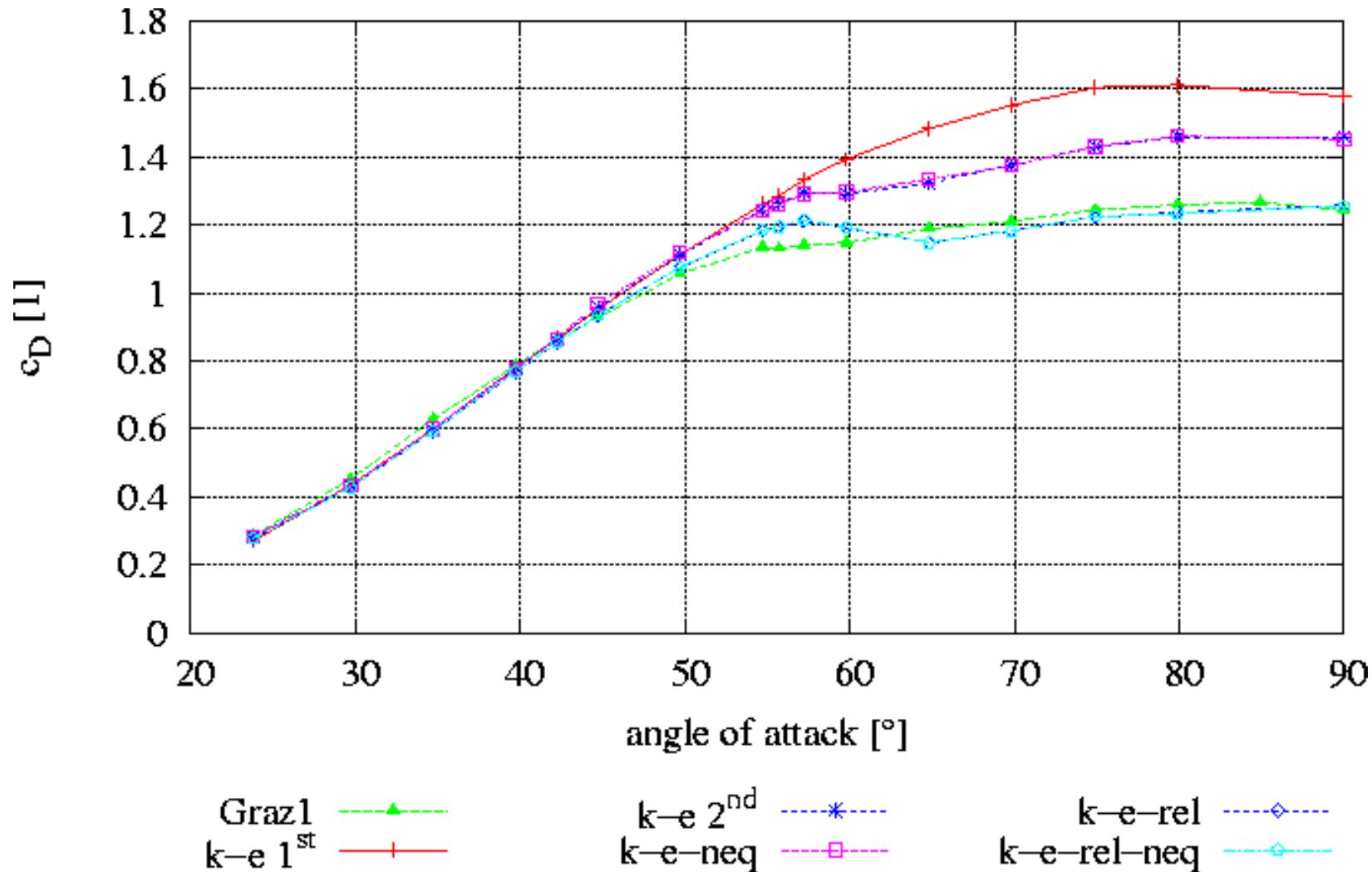
absolute
velocity
in m/s



Examples

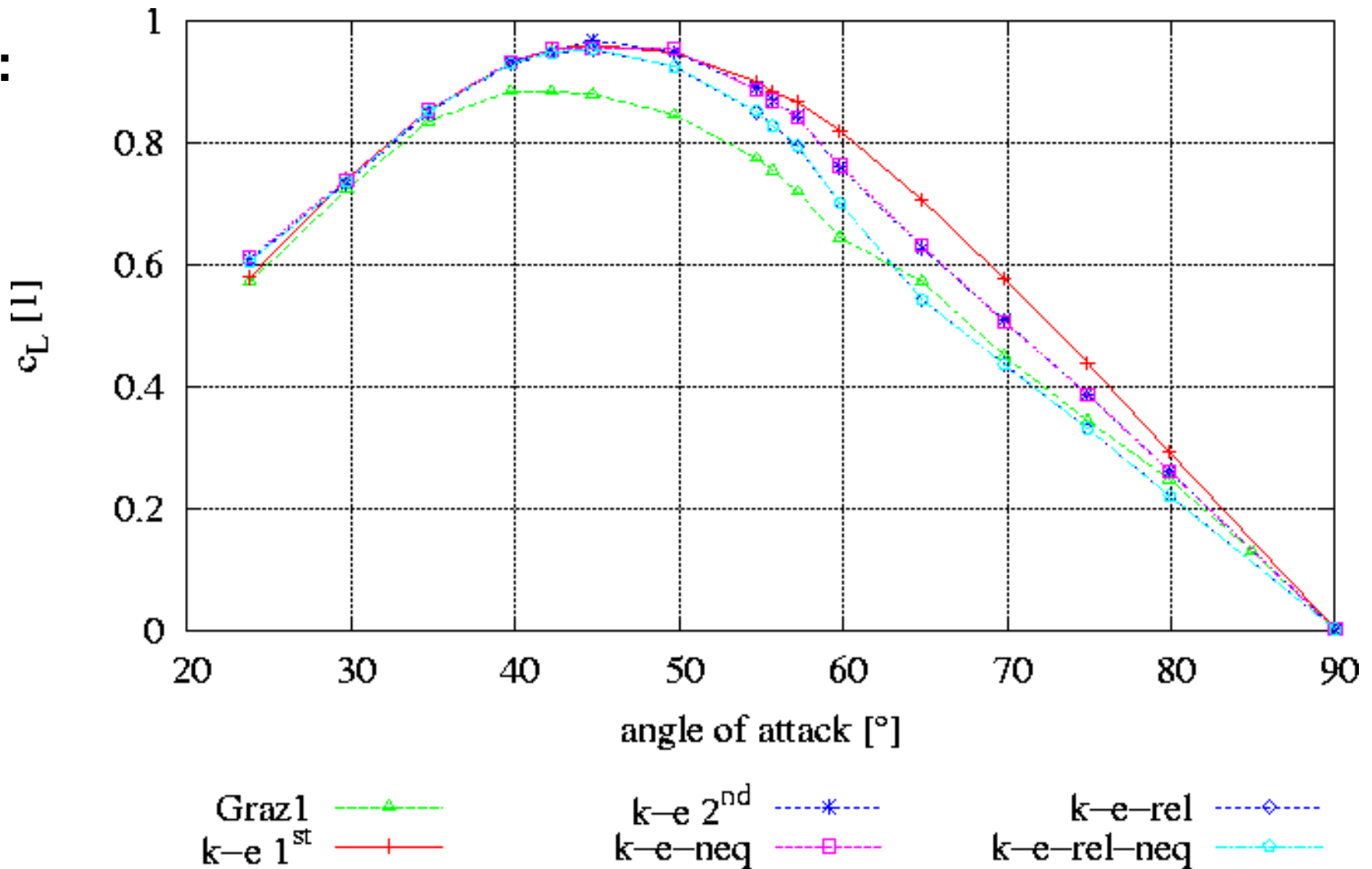
RANS of flow around a flat plate

Drag:



Examples *RANS of flow around a flat plate*

Lift:



DNS?

- Unfeasible for technically relevant engineering flows
- Restricted to scientific applications

LES?

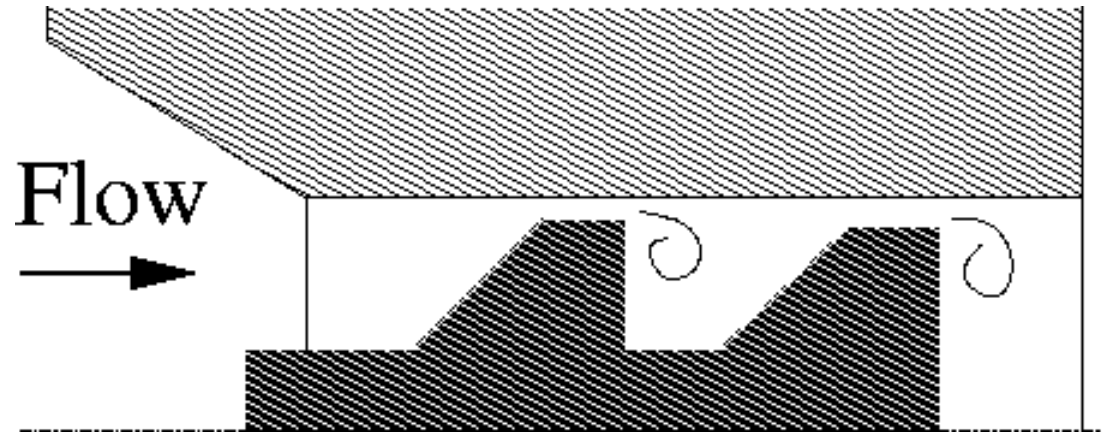
- Still computationally too expensive for many technically relevant engineering flows (aerodynamic flows, complicated geometries, etc.)
- Useful, when unsteady large scale motion has to be captured (mixing process, combustion, etc.)
- Great potential for applications in future due to increase of computer power

RANS?

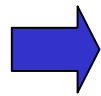
- **Method of choice in engineering flows**
- **Limited predictive capability of standard turbulence models**
- **More sophisticated turbulence models computationally expensive (but mostly still cheaper than LES !)**



Homogenizer



Complex geometry
(engineering flow)



RANS with FLUENT

models : standard $k-\epsilon$, realizable $k-\epsilon$,

Reynolds-Stress-Transport (?)